

II B.Tech I Semester Supplementary Examinations, November 2006
FLUID MECHANICS
(Chemical Engineering)

Time: 3 hours**Max Marks: 80**

Answer any FIVE Questions
All Questions carry equal marks

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1. Assuming that the rate of discharging of a centrifugal pump is dependent upon the mass density ρ of fluid, pump speed N (rpm) the diameter of the impeller D , the pressure P and the viscosity of fluid μ , show using Buckingham's II- Theorem that it can be represented by $Q = (ND^3)\phi[(gH/N^2D^2), (v/ND^2)]$
Where H = Head and v = Kinematic viscosity of the fluid. [16]
2. An incompressible fluid flows steadily through two pipes of diameter 0.15m and 0.2m which combine to discharge in a pipe of 0.3 diameter. If the average velocities in the 0.15m and 0.2m dia. Pipes are 2m/s and 3m/s respectively, find the average velocity in the 0.3m diameter pipe. [16]
3. A small capillary with an inside diameter of 2.22×10^{-3} m and a length 0.317 m is being used to continuously measure the flow rate of a liquid having a density of 875 kg/m^3 and viscosity of 1.13×10^{-3} Pa s. The pressure drop reading across the capillary during flow is 0.0655 m water of density 996 kg/m^3 . What is the flow rate in m^3/s if end effect corrections are neglected. [16]
4. The maximum velocity is measured as 3 m/s in a 0.1 m diameter tube. If the fluid flowing has a density of 1260 kg/m^3 and a viscosity of 0.9 Ns/m^2 , determine whether the flow is laminar or turbulent and determine the pressure gradient. [16]
5. Carbondioxide at one bar and 300°K is to be compressed to a pressure of 10 bar in a single stage compressor at a rate of $100 \text{ m}^3/\text{h}$. Assuming that the carbondioxide behaves as an ideal gas, calculate the temperature of the gas after compression and the work required. Take $C_p/C_v = 1.3$. [16]
6. Derive the expression for the terminal velocity of the spherical particles in the Stoke's law region. [16]
7. What is Pneumatic conveying. Explain. [16]
8. A pitot tube having a coefficient of 0.95 is inserted in the central line of a long pipe of 250mm diameter in which crude oil of density 0.9 gm/cc and viscosity 16.3 cp is flowing. Calculate the maximum velocity of the oil in the pipe if the differential pressure in the manometer is 5cm of water. [16]

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1. Explain the function of a two fluid manometer and derive the equation for pressure drop. [16]
2. An incompressible fluid flows steadily through two pipes of diameter 0.15m and 0.2m which combine to discharge in a pipe of 0.3 diameter. If the average velocities in the 0.15m and 0.2m dia. Pipes are 2m/s and 3m/s respectively, find the average velocity in the 0.3m diameter pipe. [16]
3. An incompressible fluid is flowing through a horizontal cylindrical pipe of radius r_w , show that the shear stress distribution is $[\tau_w/r_w] = [\tau/w]$. [16]
4. (a) Define hydraulic radius and equivalent diameter. Why equivalent diameter is calculated? [8]
(b) Calculate the hydraulic radius for a circular tube and for an annular flow between two concentric pipes. [8]
5. Derive the equation of energy for compressible fluid flow for adiabatic process. [16]
6. (a) Define drag force
(b) Define drag coefficient and write the expression to calculate drag coefficient.
(c) Explain frictional drag, deformation drag and form drag. [4+6+6]
7. What are the types of fluidization. Write the equations used to calculate pressure drop in fluidized beds. [16]
8. A sharp edged orifice is connected to a manometer for measuring the flow rate of brine of specific gravity 1.2 flowing through a 7.5 cm ID pipe. The maximum flow rate is not to exceed 750 lt/min. Manometer reading is 400 mm Hg .The manometer reading is 400mm Hg. Calculate the size of the orifice. [16]

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1. (a) Differentiate among manometers and mechanical gauges and give examples for each. [6]
(b) Derive the equation for differential U-Tube manometer, ignoring the reservoir and tube areas. [10]
2. Water is flowing in a pipe. At point 1, the inside diameter is 0.25m and the velocity is 2m/s. Calculate the mass flow rate, volumetric flow rate and the mass velocity. What is the velocity at point 2, where the inside diameter is 0.125m. [16]
3. Derive Hagen Poiseuille equation. [16]
4. Compute the head loss per kilo meter length of the pipe designed to carry oil of specific gravity 0.85 and kinematic viscosity $0.6 \times 10^{-3} m^2/s$ in a 15 cm diameter pipe at a rate of $0.03 m^3/s$. [16]
5. Saturated steam at 100 kpa is compressed adiabatically to 500 kpa . The compression efficiency is 80%. Determine the work required to run the compressor and the temperature of the exhaust steam. The steam is entering the compressor at a temperature of 372.8^0k , an enthalpy of 2675 kJ/kg and entropy is $7.3594 kJ/kg^0k$. [16]
6. (a) What are the different forces acting on the particle moving through the fluid.
(b) Define terminal velocity. Derive the equation for terminal velocity for gravitational settling. [6+10]
7. Write short notes on the following :
 - (a) Particulate fluidization
 - (b) Bubbling fluidization
 - (c) Spouted bed fluidization
 - (d) Slugging. [4+4+4+4]
8. It is desired to use $28.32 m^3/min$ of air (metered at a pressure of 101.3 kPa and 294.1K) in a process. This amount of air, which is at rest, enters the fan suction at a pressure of 741.7 mm Hg and a temperature of 366.3K and is discharged at a pressure of 769.6 mm Hg and a velocity of 45.7 m/s. A centrifugal fan having a fan efficiency of 60% is to be used. Calculate the brake-kW power needed. [16]

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1. Determine the dimensionless groups formed from the variables involved in the flow of fluid external to a solid body. The force exerted on the body is a function of v , l , U , and L . [16]
2. Derive the Bernoulli's equation for a frictional fluid being pumped from a point A to an elevated point B. [16]
3. Prove that the kinetic energy correction factor, $\alpha = \int u^3 ds / v^3 S$, where u is the local velocity; 'S' is the cross sectional area and 'V' is the average velocity. [16]
4. (a) Define hydraulic radius and equivalent diameter. Why equivalent diameter is calculated? [8]
(b) Calculate the hydraulic radius for a circular tube and for an annular flow between two concentric pipes. [8]
5. Air enters a convergent divergent nozzle at a temperature of $555^\circ K$ and a pressure of 20 atm. The throat area is one half that of the discharge of the divergent section. Assuming the mach number in the throat is 0.8, what are the values of the following quantities at the throat : Pressure , temperature , linear velocity , density, and mass velocity. [16]
6. Derive the expression for the terminal velocity of the spherical particles in the Stoke's law region. [16]
7. Write short notes on the following :
 - (a) Particulate fluidization
 - (b) Bubbling fluidization
 - (c) Spouted bed fluidization
 - (d) Slugging. [4+4+4+4]
8. A pitot tube with a discharge coefficient of 0.9, is connected to manometer containing water. A light oil with specific gravity of 0.8 is flowing through a pipe line of 8 cm ID. When the pitot tube is kept at the center of the pipe, the manometer reads 9 cm. Calculate the flow rate of oil if the average velocity is 80% of the maximum. [16]
